# Conceptualizing biogeochemical reactions with an Ohm's law analogy

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#### Abstract

In studying problems like plant-soil-microbe interactions in environmental biogeochemistry and ecology, one usually has to quantify and model how substrates control the growth of, and interaction among, biological organisms. To address these substrate-consumer relationships, many substrate kinetics and growth rules have been developed, including the famous Monod kinetics for single substrate-based growth, Liebig's law of the minimum for multiple-nutrient co-limited growth, etc. However, the mechanistic basis that leads to these various concepts and mathematical formulations and the implications of their parameters are often quite uncertain. Here we show that an analogy based on Ohm's law in electric circuit theory is able to unify many of these different concepts and mathematical formulations. In this Ohm's law analogy, a resistor is defined by a combination of consumers' and substrates'kinetic traits. In particular, the resistance is equal to the mean first passage time that has been used by renewal theory to derive the Michaelis-Menten kinetics under substrate replete conditions for a single substrate as well as the predation rate of individual organisms. We further show that this analogy leads to important insights on various biogeochemical problems, such as (1) multiple-nutrient co-limited biological growth, (2) denitrification, (3) fermentation under aerobic conditions, (4) metabolic temperature sensitivity, and (5) the accuracy of Monod kinetics for describing bacterial growth. We expect our approach will help both modelers and non-modelers to better understand and formulate hypotheses when studying certain aspects of environmental biogeochemistry and ecology.

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7	Key Points:
8	Ohm's law is proposed to formulate biogeochemical reactions.
9	• Ohm's law successfully models multiple substrates co-limited growth.
10 11	• Ohm's law may help building unified biogeochemical models.
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24 **Abstract**: In studying problems like plant-soil-microbe interactions in environmental 25 biogeochemistry and ecology, one usually has to quantify and model how substrates control the 26 growth of, and interaction among, biological organisms. To address these substrate-consumer 27 relationships, many substrate kinetics and growth rules have been developed, including the 28 famous Monod kinetics for single substrate-based growth, Liebig's law of the minimum for 29 multiple-nutrient co-limited growth, etc. However, the mechanistic basis that leads to these 30 various concepts and mathematical formulations and the implications of their parameters are 31 often quite uncertain. Here we show that an analogy based on Ohms' law in electric circuit 32 theory is able to unify many of these different concepts and mathematical formulations. In this 33 Ohm's law analogy, a resistor is defined by a combination of consumers' and substrates' kinetic 34 traits. In particular, the resistance is equal to the mean first passage time that has been used by 35 renewal theory to derive the Michaelis-Menten kinetics under substrate replete conditions for a 36 single substrate as well as the predation rate of individual organisms. We further show that this 37 analogy leads to important insights on various biogeochemical problems, such as (1) multiple-38 nutrient co-limited biological growth, (2) denitrification, (3) fermentation under aerobic 39 conditions, (4) metabolic temperature sensitivity, and (5) the accuracy of Monod kinetics for 40 describing bacterial growth. We expect our approach will help both modelers and non-modelers 41 to better understand and formulate hypotheses when studying certain aspects of environmental 42 biogeochemistry and ecology.

43 Plain Language Summary

Currently, scientists often use ad-hoc or empirical approaches to conceptualize and formulate
biogeochemical processes encountered in environmental sciences. Here we propose that many
biogeochemical processes can be coherently conceptualized and formulated using an analogy

based on the Ohm's law, a mathematical theory that is widely used to model electric circuits, and also the land-atmosphere exchange of water and energy. We show that this Ohm's law analogy is able to explain observations such as why microbial growth would follow the Monod kinetics, how sometimes fermentation could dominate aerobic respiration when glucose in great supply, how plant and microbes grow under multiple substrates co-limitation, etc. Since this Ohm's law analogy unifies the mathematical foundation of biogeophysics and biogeochemistry, we believe it can potentially lead to more robust land ecosystem models for projecting the climate change.

#### 54 **1. Introduction**

55 In earth system modeling, biogeochemistry strongly affects mass and energy exchanges 56 between ecosystems and the physical climate system [*Heinze et al.*, 2019]. Morphologically, 57 biogeochemistry has three pillars: biology, geophysics, and chemistry. In the context of 58 mathematical modeling, geophysics and chemistry generally have much stronger theoretical 59 foundations than biology [Brutsaert, 2005; Stumm and Morgan, 1996; Vallis, 2006], even though 60 all three are macroscale responses that emerge from atomic interactions, which in an ideal (but 61 impractical) scenario can be predicted by solving the Schrödinger equation of all atoms together (so that arguably they all are subtopics of physics) [Feynman et al., 2011b]. 62

In seeking a better understanding of ecological dynamics, e.g., competition and symbiosis, mathematical formulations of the consumer-substrate relationship are essential for both theoretical modeling and interpreting empirical experiments [*Tilman*, 1982]. In the past, three approaches have been used to obtain such relationships. The first approach is by fitting certain empirical response functions to observational data [e.g., *Monod*, 1949]. The second approach is based on an ad-hoc heuristic conceptualization of the problem, e.g., the logistic equation was derived by adding a quadratic term to dissipate the exponential growth of a

70 population when Pierre-Francois Verhulst (1804-1849) was helping his teacher Alphonse 71 Quetelet (1975-1874) to model human population dynamics [*Cramer*, 2002]. The third approach 72 is based on systematic applications of some theory, such as the law of mass action [Atkins et al., 73 2016], statistical mechanics [Ma, 1985], and renewal theory [Doob, 1948]. Notably, Michaelis-74 Menten kinetics (and some of its extensions) can be derived by applying any of these theories 75 (see reviews in [Kooijman, 1998; Swenson and Stadie, 2019; Tang and Riley, 2013; 2017]), with 76 the renewal theory even being able to show that Michaelis-Menten kinetics is the statistical mean 77 of the stochastic description of a single enzyme molecule processing the substrate molecules 78 [English et al., 2006; Reuveni et al., 2014].

79 Compared to the empirically-based and ad-hoc approaches, which generally provide 80 limited understanding of the processes implied by the parameters, theory-based approaches have 81 the advantage of linking various related albeit fragmented knowledge (that is abstracted from a 82 much wider range of observations compared to the limited amounts of observational data used by 83 the empirically-based approaches), thereby enabling a deeper understanding of the processes and 84 systems of interest. For instance, when law of mass action is used to derive the Michaelis-85 Menten kinetics, using the related theory of chemical reaction rates (e.g., Smoluchowski's 86 diffusion model of chemical reaction [von Smoluchowski, 1917]), Tang and Riley [2019b] were 87 able to upscale the microbially-enabled reactions from one permease to a single bacteria cell and 88 then to a representative soil volume ( $\sim O(1 \text{ cm}^3)$ ), and used the results to explain why substrate 89 affinity parameters are highly variable in soil. Additionally, the theory-based approach has been 90 used to derive the temperature response function of microbial activity [Ghosh and Dill, 2010], 91 and to explain why Michaelis-Menten kinetics are more appropriate for microbial uptake of

92 small molecules, while reverse Michaelis-Menten kinetics are more appropriate for enzyme
93 degradation of organic polymer particles [*Tang and Riley*, 2019a].

94 In this paper, we first introduce an analogy that uses the Ohms' law from electric circuit 95 theory to interpret the resource-consumer relationship. Similar analogies have been widely used 96 by land models to represent the physics of land-atmosphere exchanges of water, gases, and 97 energy [e.g., Lawrence et al., 2019; Riley et al., 2011; Shuttleworth and Wallace, 1985; Wu et 98 al., 2009]. (So that in a certain sense, the Ohm's law is unifying all three aspects of 99 biogeochemistry into physics.) We then exploit this analogy to explain several interesting 100 biogeochemical phenomena that are observed in various context. We conclude the paper with 101 recommendations of other potential applications of this analogy. 102 Although the example problems below are solved with the Ohm's law analogy, we note

104 kinetics [*Tang and Riley*, 2013] or the synthesizing unit plus ECA (SUPECA) kinetics [*Tang and* 

that they can all be solved using the more accurate Equilibrium Chemistry Approximation (ECA)

105 *Riley*, 2017]. However, the Ohms' law analogy proposed here is more intuitive and can provide

106 an alternative to the ECA and SUPECA kinetics in formulating biogeochemical models.

**107 2 Methods** 

103

# 108 **2.1 A brief review of Ohm's law and circuit theory**

109 We below briefly review Ohm's law and the theory of series and parallel resistor circuits.

110 More detailed descriptions of circuit theory can be found in *Feynman et al.* [2011a].

Ohm's law describes the relationship between voltage (V), electric current (I), and
resistor (r):

$$I = \frac{v}{r}.$$
 (1)

113 To simplify the presentation, we assume that all variables are properly defined with their

114 international units.

115 For a series concatenation of resistors  $r_i$ , application of Ohm's law yields

$$I = \frac{v}{\sum_j r_j}.$$
(2)

116 For a parallel concatenation of resistors  $r_i$ , application of Ohm's law leads to

$$I = V\left(\sum_{j} \frac{1}{r_j}\right),\tag{3}$$

and the electric current through each resistor is

$$I_j = \frac{v}{r_j}.$$
(4)

118 From equations (3) and (4), we can further derive

$$\frac{I_j}{I} = \frac{1}{1 + \left(\sum_{l \neq j} \frac{r_j}{r_l}\right)},\tag{5}$$

119 which states that when all other resistors are fixed, the fraction of current through  $r_i$  increases

- 120 with decreasing  $r_i$ . We will see later that this inference is very useful to explain shifts in
- 121 metabolic pathways in biological organisms.

# 122 2.2. Michaelis-Menten kinetics interpreted with Ohm's law

123 Michaelis-Menten kinetics represents the single-enzyme catalyzed single-substrate

124 reaction velocity v as

$$v = \frac{v_{max}ES}{K+S},\tag{6}$$

125 where, in the original application by *Michaelis and Menten* [1913],  $v_{max}$  is the maximum

- specific hydrolysis rate enabled by the invertase and *E*, *S*, and *K* are enzyme concentration,
- 127 substrate concentration, and half saturation coefficient, respectively. We note that, for enzymes,
- 128 *K* also includes contributions from the dissociation process [e.g., *Briggs and Haldane*, 1925].

129 By defining  $k_f = v_{max}/K$ , equation (6) can be rewritten as

$$v = \frac{E}{\frac{1}{v_{max}} + \frac{K}{v_{max}S}} = \frac{E}{\frac{1}{v_{max}} + \frac{1}{k_fS}}.$$
(7)

130

We then note that equations (7) and (1) are of the same form. Therefore, for Michaelis-131 Menten kinetics, if we apply the Ohm's law analogy by regarding E as voltage and v as current, 132 the corresponding resistance is

$$r = \frac{1}{v_{max}} + \frac{1}{k_f s} = r_E + r_S,$$
(8)

where  $r_E$  represents the resistance as an intrinsic property (i.e., a kinetic trait) of the enzyme, and 133 134  $r_{\rm S}$  represents the resistance introduced by the effective substrate delivery rate towards the enzyme. Further,  $r_E$  and  $r_S$  are of the unit of time, where (in the renewal theory [e.g., *Kooijman*, 135 1998])  $r_E$  is the mean time for the enzyme to convert the enzyme-bound substrate molecules into 136 137 product molecules and  $r_s$  is the mean time for the substrate molecules to approach the enzyme 138 molecule and form enzyme-substrate complexes. Together, r is the mean first passage time of 139 the stochastic description of how a single enzyme catalyzes the degradation of the substrate 140 molecules [e.g., Kooijman, 1998; Ninio, 1987; Qian, 2008]. In particular, in many reactions, k<sub>f</sub> 141 is approximately proportional to the substrate diffusivity [Alberty and Hammes, 1958; Chou and Jiang, 1974], such that  $k_f S$  is the diffusive substrate flux sensed by enzyme molecules. We then 142 143 observe that  $r_s$  increases with the decrease of diffusive substrate flux, which can result from 144 lower substrate concentration, or lower diffusivity (due to tortuosity, adsorption, or lower 145 moisture in porous media like soil). 146 That the resistance r in equation (8) is of the time unit has also motivated some

147 researchers to apply the time budget idea to derive predator-prey relationships [e.g., *Holling*,

1959; Murdoch, 1973], where  $r_E$  is referred as the mean time spent on handling the prey, and  $r_S$ 148

149 is the mean time for the predator to encounter the prey. However, few studies have pointed out 150 the linkage between the time-budget analysis and Ohm's law, except that, based on a suggestion 151 by Thomsen et al. [1994], Almeida et al. [1997] made an analogy of the membrane electron-152 transport chain to an electric circuit, and successfully used it to model denitrification. Recently, 153 this method has been used by Domingo-Felez and Smets [2020] to build the Activated Sludge 154 Model-Electron Competition (ASM-EC) model, which demonstrated the efficacy of this analogy 155 in constructing robust biogeochemical models. Further, we noticed that the molecular biology of 156 membrane electron transport chains and redox reactions are quite similar to the working 157 principles of chemical batteries [Schmidt-Rohr, 2018], thereby motivating us to explore more 158 extensively the applicability of Ohm's law analogy below.



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are reversed (such as for enzyme hydrolysis of polymeric organic matter; [*Tang and Riley*,

171 2019a]). (We note that the ECA kinetics are able to more accurately handle the wide range of

172 substrate abundances with respect to enzymes [*Tang*, 2015].) We next show how the Ohm's law

173 analogy will help us formulate biogeochemical kinetics for various situations.

174 **3. Applications** 

## 175 **3.1** Series resistor circuit-based formulation of chain-like enzyme reactions

176 Many metabolic pathways consist of a chain of reactions. Such examples include the 177 Calvin-cycle (in photosynthesis), membrane electron transport chain, glycolysis, citric acid 178 cycle, etc., and note that most of these reaction pathways involve cofactors [Madigan et al., 179 2009; Taiz and Zeiger, 2006]. Nonetheless, assuming that at each step the enzyme and its co-180 factor together form an integrated enzyme unit to process the substrate delivered from a prior 181 step, and the whole chain of enzymatic reactions are in detailed balance (i.e., the whole chain is 182 in steady state without overflow [*Cao*, 2011], an assumption that is often made in flux balance 183 models [Orth et al., 2010]), we can then use the series circuit analogy to calculate the overall 184 enzyme kinetics straightforwardly. According to the schema for this configuration (Figure 1b), 185 when the whole enzyme chain is taken as a catalysis unit, the abundance of enzyme at the first 186 step represents the voltage of the battery, and the total resistance is

$$r_{chain} = \left(\sum_{j=1}^{N} r_{E,j}\right) + r_{S,1} = r_E + r_{S,1},\tag{9}$$

187 where  $r_{E,j} = v_{max,j}^{-1}$  such that the first right hand side term is the total resistance represented by 188 the maximum catalysis rate of the overall enzyme chain, and  $r_{S,1} = (k_{f,1}S_1)^{-1}$  is the resistance 189 due to the incoming substrate flux to the first enzyme in the chain. For the overall chain, the 190 specific reaction rate for substrate processing is then

$$\frac{v_{chain}}{E_{chain}} = \frac{1}{r_{chain}} = \frac{\left(\sum_{j=1}^{N} v_{max,j}^{-1}\right)^{-1} S_1}{\frac{K_1}{v_{max,1}(\sum_{j=1}^{N} v_{max,j}^{-1})} + S_1} \quad , \tag{10}$$

191 where  $K_1 = v_{max,1}/k_{f,1}$ . Equation (10) can be simplified as

$$\frac{v_{chain}}{E_{chain}} = \frac{v_{max,chain}S_1}{K_{chain}+S_1},\tag{11}$$

192 with

$$v_{max,chain} = \left(\sum_{j=1}^{N} v_{max,j}^{-1}\right)^{-1} < \min_{j} \{v_{max,j}\},\tag{12}$$

193 and

$$K_{chain} = \frac{K_1}{v_{max,1}\left(\sum_{j=1}^N v_{max,j}^{-1}\right)} = \frac{K_1}{1 + \sum_{j=2}^N v_{max,1}/v_{max,j}}.$$
(13)

From equation (10), we assert that an enzyme chain is equivalent to an enzyme unit with kinetic traits  $v_{max,chain}$  and  $K_{chain}$ . Moreover, from equations (12) and (13), we infer that increasing the chain length decreases the overall reaction rate  $v_{max,chain}$  (which is even slower than the slowest step) and the half saturation coefficient  $K_{chain}$  of the enzyme chain.

198 Several interesting inferences can be additionally drawn from equations (9)-(13). First, 199 the second law of thermodynamics suggests that a thermal engine has higher thermodynamic 200 efficiency when it runs slower (and the highest efficiency can only be achieved when the system 201 is in thermodynamic equilibrium, i.e., not running at all [Salamon et al., 2001]). Since a longer 202 reaction chain slows down the overall transformation rate from a given substrate to its final 203 product, (as an example,) application of the above equations to electron transport chains leads us 204 to assert that a longer chain will likely be thermodynamically more efficient (this argument 205 echoes the Ladder theorem in finite time thermodynamics; [Salamon et al., 2017]). In contrast, 206 shorter electron transport chains imply faster use of substrates even though they result in less 207 efficient substrate use. Therefore, the length of electron transport chains can characterize the

208 tradeoff between substrate use rate and substrate use efficiency, an important selection factor for 209 organisms during their evolution. Indeed, in one chemostat based study, Chen et al. [2017] found 210 that Vibrionales bypass respiratory complex III to consume part of the oxygen using a 211 cytochrome bd terminal oxidase to speed up growth, but the bioenergetic efficiency becomes 212  $\sim$ 32% as compared to  $\sim$ 80% for the longer canonical respiratory chain. Similarly, observations 213 indicate that the less efficient fermentation pathway which has fewer enzymes involved is faster 214 than the aerobic respiration pathway that has many more enzymes involved (thus is longer and 215 more efficient; [Madigan et al., 2009]). We will later (in section 3.5) use the parallel circuit 216 analogy to explain why such bypassing of more efficient pathways will occur under substrate 217 abundant conditions.

The second inference to be made is about the temperature sensitivity of parameters  $v_{max,chain}$  and  $K_{chain}$ . In the simplest one-step case,  $v_{max,chain}$  equals  $v_{max,1}$ , and  $K_{chain}$  equals  $K_1$ . According to transition state theory [e.g., *Eyring*, 1935],  $v_{max,1}$  would have the following temperature dependence,

$$v_{max,1} = v_{max,1,ref} T \cdot exp\left(-\frac{\Delta G_1}{RT}\right),\tag{14}$$

where  $v_{max,1,ref}$  is some reference reaction rate, *T* is temperature,  $\Delta G_1$  is the Gibbs energy of activation, and *R* is the universal gas constant. Similarly, for a reaction pathway consisting of a chain of enzymes, each  $v_{max,j}$  will have a temperature dependence similar to that in equation (14), that is

$$v_{max,j} = v_{max,j,ref} T \cdot exp\left(-\frac{\Delta G_j}{RT}\right),\tag{15}$$

which when entered into equation (12),  $v_{max,chain}$  will then be of the form

$$v_{max,chain} = \left[\sum_{j=1}^{N} \left( v_{max,j,ref}^{-1} exp\left(\frac{\Delta G_j - \Delta G_1}{RT}\right) \right) \right]^{-1} T \cdot exp\left(-\frac{\Delta G_1}{RT}\right).$$
(16)

227 Therefore, if  $(\Delta G_j - \Delta G_1)/(RT) \ll 1$ , the temperature dependence of  $v_{max,chain}$  will be 228 approximately like that in equation (14).

The temperature dependence of  $K_1$  is determined by the temperature dependencies of 229 230  $v_{max,1}$  and  $k_{f,1}$ . Inside the microbial cytoplasm and cell membrane (and also for whole microbial cells in most natural environments),  $k_{f,1}$  is closely related to diffusivity [Madigan et al., 2009]. 231 Thus, according to the Stokes-Einstein equation of diffusivity  $(D = (k_B T)/(6\pi \eta a))$ , where  $k_B$  is 232 233 the Boltzmann constant,  $\eta$  is the dynamic viscosity, and a is the radius of the spherical particle) [Feynman et al., 2011c],  $k_{f,1}$  can be approximated with a linear dependence on temperature 234 divided by the temperature sensitivity of  $\eta$  (which is  $exp(B/(T - T_{VF}))$ ), where B and  $T_{VF}$  are 235 236 empirical parameters, according to the semi-empirical Vogel-Fulcher-Tamman-Hesse equation [Garcia-Colin et al., 1989]). When the temperature dependence of  $k_{f,1}$  is combined with the 237 Eyring-type temperature dependence of  $v_{max,1}$ , the definition of  $K_1$  (=  $v_{max,1}/k_{f,1}$ ) suggests 238 that its temperature dependence is of the Arrhenius type (because  $exp(B/(T - T_{VF}))$ ) of the 239 240 viscosity is very similar to the Arrhenius equation, and the linear temperature dependence of  $k_{f,1}$ cancels out the linear part of the temperature dependence of  $v_{max,1}$ ). Once again, if 241  $(\Delta G_i - \Delta G_1)/(RT) \ll 1$ ,  $K_{chain}$  will probably have an Arrhenius-type temperature sensitivity as 242 243 well.

When the above inferences are put into equation (11), we can then infer the temperature dependence of  $v_{chain}$ . From chemical thermodynamics, the temperature dependence of  $v_{chain}$ depends on chemical kinetics (as characterized by the Michaelis-Menten term, i.e.,  $\frac{v_{max,chain}S_1}{K_{chain}+S_1}$  in this example) and thermodynamics (as a function of the Gibbs free energy) of the enzyme catalyzed reaction. However, because enzymes are proteins, their conformational states are also

- temperature dependent [Murphy et al., 1990]. Thermodynamically, the undenatured (aka
- 250 catalytically active) fraction of an enzyme population of length  $n_x$  (as measured by the number
- of amino acid residues) can be described as [Murphy et al., 1990]

$$f_{ax} = \frac{1}{1 + exp\left(-\frac{n_X \Delta G_X}{RT}\right)},\tag{17}$$

252 where

$$\Delta G_x = \Delta H^* - T\Delta S^* + \Delta C_p [(T - T_H^*) - T ln(T/T_S^*)], \qquad (18)$$

253 and

$$\Delta C_p = -46.0 + 30(1 - 1.54n_x^{-0.268})N_{CH,x},\tag{19}$$

254 with heat capacity  $\Delta C_P$  defined as the energy required to reorganize the water molecules 255 surrounding the protein [Ratkowsky et al., 2005].  $\Delta C_P$  increases with the non-polar accessible 256 area of the molecule, as measured by  $N_{CH,x}$ , the average number of non-polar hydrogen atoms per amino acid residue.  $\Delta C_p$  also measures the hydrophobic contribution, with higher values 257 258 implying higher hydrophobicity (and notice that greater  $N_{CH,x}$  implies higher hydrophobicity). 259 Other parameters include  $\Delta S^*$  as the enthalpy change at  $T_S^*$  (the convergence temperature for entropy) and  $\Delta H^*$  as the enthalpy change at  $T_H^*$  (the convergence temperature for enthalpy), 260 261 which can be considered to be constant under environmental conditions [e.g., Ratkowsky et al., 262 2005]. Assuming  $N_{CH,x}$  and  $n_x$  can be obtained from proteomic data for each type of enzyme [e.g., Sawle and Ghosh, 2011], we can then calculate  $f_{ax,j}$  for all enzymes involved in the chain. 263 Therefore, putting together the kinetic, thermodynamic, and catalytically active enzyme fraction 264 265 functions, we obtain

$$\nu_{chain} = \frac{\nu_{max,chain}S}{K_{chain}+S} F_T \prod_j f_{ax,j}, \tag{20}$$

where the thermodynamic temperature dependence of the reaction is

$$F_T = 1 - exp\left(-\frac{\Delta G_{reac}}{RT}\right),\tag{21}$$

with  $\Delta G_{reac}$  being the Gibbs free energy of the overall reaction being catalyzed, which is defined by the chemical activity of initial substrates and final products [e.g., *Jin and Bethke*, 2007].



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Figure 2. a. type-1 circuit schema for redox-type reaction; b. type-2 circuit schema for redoxtype reaction; c. circuit schema for parallel resistor-based schema for competitive enzymatic
reactions. Type-1 and Type-2 schema are equivalent, and are not differentiated in the Ohm's law
analogy. Symbols are explained in the main text.

274 Unless equation (20) is applied to organisms capable of growing on alternative electron 275 acceptors or donors, and the system is undergoing fast transition in redox status (e.g., at the depth 276 of the soil water table),  $F_T$  is very close to 1, and can be ignored. Therefore, the temperature dependence of  $v_{chain}$  is dominated by the kinetic term (i.e., that of the Michaelis-Menten term) 277 and the temperature dependent fraction of active enzymes  $(\prod_i f_{ax,i})$ . The kinetic term increases 278 279 with temperature, while the fraction of active enzymes first increases, then decreases with 280 temperature. The overall temperature sensitivity of the reaction chain will be of the form 281 predicted by the macromolecular rate theory (MMRT) (with fine tuning from substrate 282 availability through the kinetic term which MMRT does not consider) [Arcus et al., 2016; 283 Schipper et al., 2014]. Therefore, for a population of cells that are not under substrate limitation

and steadily growing (so that one metabolic pathway dominates the metabolism), one should
expect a MMRT type temperature dependence of the metabolic rates. This thus explains why *Ratkowsky et al.* [2005] was able to use the following equation to model bacterial growth rates
under unlimited substrate supply:

$$g = \frac{cTexp(-\Delta H_A/RT)}{1 + exp\left(-\frac{n}{RT}(\Delta H^* - T\Delta S^* + \Delta C_p[(T - T_H^*) - Tln(T/T_S^*)])\right)},$$
(22)

where *g* is growth rate, *c* is an empirical constant, and  $\Delta H_A$  is substrate dependent activation energy. However, unlike it was historically assumed that properties of some single control enzyme determine the overgrowth [*Johnson and Lewin*, 1946], here *n* and  $\Delta C_p$  represent mean values of protein length and their thermal property, under possible influences from other molecules, such as phospholipids [e.g., *Mansy and Szostak*, 2008].

# 293 **3.2 Series resistor-based formulation of enzyme catalyzed redox reactions**

Many biogeochemical processes are of the redox type, including photosynthesis, aerobic respiration, nitrification, anaerobic denitrification, etc. [*Madigan et al.*, 2009; *Taiz and Zeiger*, 2006]. Basically, enzyme catalyzed redox reactions facilitate electron transfers from electron donors to electron acceptors. This process can be summarized with the schema Figure 2a that has one resistor representing electron donors ( $r_{s,edon}$ ), and the other resistor ( $r_{s,eacc}$ ) representing electron acceptors, with the enzyme being the battery. By applying the Ohm's law analogy, the reaction rate is

$$v = \frac{E}{r_{eacc} + r_{edon}},\tag{23}$$

301 where 
$$r_{eacc} = \frac{1}{v_{max,eacc}} + \frac{1}{k_{f,eacc}S_{eacc}}$$
, and  $r_{e,acc} = \frac{1}{v_{max,edon}} + \frac{1}{k_{f,edon}S_{edon}}$ . When the two are

302 combined, equation (23) can be rewritten as

$$v = \frac{E}{r_E + \frac{1}{k_{f,eacc}S_{eacc}} + \frac{1}{k_{f,edon}S_{edon}}}.$$
(24)

303 with 
$$r_E = \frac{1}{v_{max,eacc}} + \frac{1}{v_{max,edon}}$$
,  $r_{S,eacc} = \frac{1}{k_{f,eacc}S_{eacc}}$ , and  $r_{S,edon} = \frac{1}{k_{f,edon}S_{edon}}$ . We note that in

this series resistor-based formulation, the total resistance (or mean first passage time) does not include the discount resulting from the concurrent binding of electron donors and acceptors to the enzyme (i.e., configuration Figure 2b is as good as Figure 2a, and they have the same resistance). However, this discount can be incorporated by renewal theory (or law of mass action), which leads to the synthesizing unit (SU) model [*Kooijman*, 1998] below

$$v = \frac{E}{r_E + \frac{1}{k_{f,eacc}S_{eacc}} + \frac{1}{k_{f,edon}S_{edon}} - \frac{1}{k_{f,eacc}S_{eacc} + k_{f,edon}S_{edon}}}.$$
(25)

309 Compared to equation (24), the SU model (i.e., equation (25)) is numerically more 310 accurate (in approximating the law of mass action, the standard method that deals with 311 biogeochemical reactions [Koudriavstev et al., 2001]). Equations (24) and (25) differ by the additional term  $-1/(k_{f,eacc}S_{eacc} + k_{f,edon}S_{edon})$  that accounts for the co-existence of schemas 312 313 in Figure 2a and Figure 2b. 314 Equation (24) was derived as early as in *Alberty* [1953], and is called the additive model. 315 It was found as the superior formulation to model multiple nutrient limitations of microbial and 316 plant growth in O'Neill et al. [1989] (where electron donors and acceptors are replaced with

317 complementary nutrients, such as nitrogen and phosphorus). In particular, the additive model

318 equation (24) can be extended to include arbitrary number of nutrients:

$$\nu = \frac{E}{r_E + \sum_j \frac{1}{k_{f,j} S_j}}.$$
(26)

319 where  $S_i$  can be essential nutrients including carbon, nitrogen, phosphorus, potassium,

320 chloronium, etc. *Smith* [1976; 1979] used equation (26) to model plant growth and microbial

321 growth under carbon, nitrogen, phosphorus, and potassium co-limitation. Based on past 322 successful applications [Franklin et al., 2011; Kooijman, 1998], the SU model (i.e., equation 323 (25)) may be argued as mathematically more rigorous than the series resistor-based additive 324 model (i.e., equation (24) or (26)). However, given the usually significant uncertainty of 325 ecological data, the series resistor-based additive model may be equally good. Indeed, when we 326 applied both the SU model and the resistor-based additive model to the measured algal growth 327 rates under various levels of phosphorus and vitamin B<sub>12</sub> additions [Droop, 1974], both models 328 can be satisfyingly calibrated with respect to the growth data (Figure 3a and b). Further, when 329 the normalized growth rates are contoured as a function of the normalized substrate fluxes, the 330 SU and resistor-based additive models show very similar growth patterns (Figure 3c and d). The 331 SU model and additive model also performed equally well for the plant growth data from Shaver 332 and Melillo [1984] (Figure 4). Moreover, when the SU model and additive model are used to 333 model aerobic heterotrophic respiration using the parameterization from *Tang and Riley* [2019b], 334 we once again find the two models resulted in very similar goodness of fit with respect to the 335 measurements (Figure 5). These lines of evidence suggest that one can probably use these two 336 models alternatively. In particular, both can be a substitute for Liebig's law of the minimum that 337 is used by most existing biogeochemical models [Achat et al., 2016].

Additionally, we note that equation (26) can be extended into a photosynthesis model to replace the Farquhar or Collatz model that is formulated based on Liebig's law of the minimum, which has to arbitrarily smooth the abrupt transitions from one limiting process to another [e.g., *Collatz et al.*, 1990; *Collatz et al.*, 1992; *Farquhar et al.*, 1980; *Kirschbaum and Farquhar*,

342 1984]. In this context, we contend that it is possible to use the same kinetics to formulate models

343 of plant photosynthesis, microbial substrate dynamics, and biomass growth, a strategy that will



344 likely enhance the mathematical coherence in modeling plant-soil-microbial interactions.

Figure 3 **a** comparison of the calibrated synthesizing unit (SU) model prediction for the algal growth rates data from *Droop* [1974]; **b** same as **a** but from the calibrated resistor-based additive model; **c** contour of normalized growth rate as a function of normalized fluxes of substrates A and B for the SU model; **d** same as **c** but for the resistor-based additive model. The additive model is presented as equation (24), and the SU model is presented as equation (25). Model parameters are in Table S1 of the supplemental material.



353Measured plant biomass increase (g/pot)Measured plant biomass increase (g/pot)354Figure 4 a SU model predicted vs measured plant growth; b Additive model predicted vs

measured plant growth. The data is from *Shaver and Melillo* [1984]. Model parameters are in
 Table S1 of the supplemental material.



357

Figure 5. Left panels are SU model-based prediction of respiration-soil-moisture relationship; right panels are based on the resistor-based additive model. The two models used identical parameters, which are detailed in *Tang and Riley* [2019b]. The statistics for model-data fitting (in terms of linear regression and root mean square error) between two models are identical to 0.01

362 (see Table S2 of the supplemental material).

# 363 **3.3 Parallel resistor-based formulation of competitive kinetics**

364 Many microorganisms can feed on multiple substrates. For example, *E.coli* and yeasts are

- able to perform both aerobic and anaerobic respiration [e.g., Dashko et al., 2014; Unden and
- 366 Bongaerts, 1997]. Meanwhile, some enzymes can react on different substrates, e.g., enzyme
- 367 ribonuclease is able to degrade various RNA molecules [*Etienne et al.*, 2020]. Thus, we next
- 368 show that such problems can be formulated using the parallel circuit (plus one series resistor)
- analogy.

**a**  

$$r_{E,N,eacc}$$

$$r_{S,N,eacc} = 1/(k_{f,N,eacc}S_{N,eacc})$$

$$r_{E,1,eacc}$$

$$r_{S,1,eacc} = 1/(k_{f,1,eacc}S_{1,eacc})$$

$$r_{E,1,edon}$$

$$r_{S,1,edon} = 1/(k_{f,1,edon}S_{1,edon})$$

$$r_{E,L,edon}$$

$$r_{S,L,edon} = 1/(k_{f,L,edon}S_{L,edon})$$

$$r_{E,M,edon}$$

$$r_{S,M,edon} = 1/(k_{f,M,edon}S_{M,edon})$$
**b**  

$$r_{C_{2}} = 1/f_{O2}$$

$$r_{etc}$$

$$r_{cac}$$

$$r_{S} = 1/f_{S}$$

$$r_{fm}$$

$$r_{S} = 1/f_{S}$$

370

Figure 6. a mixed resistor circuit schema for redox reactions with alternative electron donors and
acceptors; b circuit schema for the parallel fermentation and aerobic respiration pathways.
Symbols are explained in the main text.

We first formulate the competitive Michaelis-Menten kinetics using the schema in Figure

375 2c. For this case, the total resistance is

$$r = r_E + r_S = r_E + \left(\sum_j (r_{E,j} + r_{S,j})^{-1}\right)^{-1},$$
(27)

376 where  $r_{S,i}^{-1} = k_{f,i}S_i$ , and  $r_{E,i}$  is the resistance due to preprocessing of substrate  $S_i$  before it is

- 377 handed to the central enzyme *E* (i.e., the enzyme that products of all substrates have to pass
- 378 through), and  $r_E = 1/v_{max,E}$  is the resistance due to the maximum substrate processing rate of

the central enzyme (which for redox-reactions could be determined by the time spent on

380 processing the electron donors if  $S_j$  here are electron acceptors). If  $r_{E,j} = 0$ , which is usually

assumed for competitive Michaelis-Menten kinetics, the second term  $r_S$  becomes  $(\sum_j k_{f,j} S_j)^{-1}$ ,

and the reaction velocity is

$$\nu = \frac{E}{r} = \frac{E}{\frac{1}{\nu_{max}} + (\sum_{j} k_{f,j} S_{j})^{-1}},$$
(28)

and the corresponding flux through pathway *j* is

$$v_{j} = \frac{vr_{S}}{r_{S,j}} = v \frac{k_{f,j}S_{j}}{\sum_{l}k_{f,l}S_{l}} = E \cdot \frac{v_{max}S_{j}/K_{j}}{1 + \sum_{l}S_{l}/K_{l}},$$
(29)

where  $K_j = v_{max}/k_{f,j}$ . It is easy to see that  $v_j$  is the reaction velocity computed from the competitive Michaelis-Menten kinetics. We note that equation (29) is meaningful only when pathway *j* produces new molecules. However, even for inhibitors, whose binding to enzymes does not produce new molecules, if we regard dissociation as a way of producing new molecules, then equation (29) is still mathematically meaningful.

# 389 **3.4** Mixed series and parallel resistor-based formulation of redox reactions of alternative

# 390 electron donors and acceptors

Many microorganisms (such as denitrifying bacteria; e.g., *Robertson and Groffman*[2015]) are able to grow on different electron donors and acceptors. Such problems can be solved
using the SUPECA kinetics [*Tang and Riley*, 2017]. Below we formulate it using the schema of
mixed series and parallel resistors.

Based on the schema in Figure 6a, the total resistance is

$$r = r_{edon} + r_{eacc} = \left(\sum_{l} r_{l,edon}^{-1}\right)^{-1} + \left(\sum_{j} r_{j,eacc}^{-1}\right)^{-1},\tag{30}$$

396 where the resistance for electron donors is

$$r_{l,edon} = r_{E,l,eacc} + r_{S,l,eacc} = \frac{1}{v_{max,l,eacc}} + \frac{1}{k_{f,l}S_{l,eacc}},$$
(31)

397 and the resistance for electron acceptors is

$$r_{j,eacc} = r_{E,j,edon} + r_{S,j,edon} = \frac{1}{v_{max,j,edon}} + \frac{1}{k_{f,j,edon}S_{j,edon}}.$$
(32)

398 Accordingly, the corresponding reaction flux through electron donor j is

$$v_{j,edon} = \frac{E}{r} \frac{r_{edon}}{r_{j,edon}} = \frac{E}{r_{j,edon}} \frac{r_{edon}}{r_{edon} + r_{eacc}},$$
(33)

399 while the corresponding reaction flux through electron acceptor j is

$$v_{j,eacc} = \frac{E}{r} \frac{r_{eacc}}{r_{j,eacc}} = \frac{E}{r_{j,eacc}} \frac{r_{eacc}}{r_{edon} + r_{eacc}}.$$
(34)

400 Now considering an application that involves two electron acceptors, e.g., nitrate and nitrite in

401 denitrification, we have

$$\frac{1}{r_{eacc}} = \frac{1}{r_{NO3}} + \frac{1}{r_{NO2}},\tag{35}$$

402 which when combined with equation (34) leads to

$$v_{NO3} = \frac{E}{r_{NO3} + r_{edon} + r_{edon} r_{NO3} / r_{NO2}},$$
(36)

403 and

$$\nu_{NO2} = \frac{E}{r_{NO2} + r_{edon} + r_{edon} r_{NO2} / r_{NO3}},$$
(37)

404 which are just the equations (10) in *Almeida et al.* [1997] that have been successfully used to fit

405 the measurement of denitrification rates from *Almeida et al.* [1995]. With proper number of

406 resistors, the denitrifier model by *Domingo-Felez and Smets* [2020] can also be easily recovered

407 from equations (30)-(34).

## 408 **3.5 Other potential applications of the Ohm's law analogy**

Besides the applications described above, we below use the Ohm's law analogy to derivesome quite interesting results.

411 First, we will explain why fermentation can occur even when there is still oxygen to 412 support the energetically more efficient aerobic respiration. Such a phenomenon is called the 413 Warburg effect (i.e., lactate producing aerobic fermentation) in proliferating mammalian cells (a 414 phenomenon important to the understanding of cancer development), or the Crabtree effect (i.e., 415 ethanol fermentation) of unicellular yeast Sacchamoyces cerevisiae [e.g., de Alteriis et al., 2018]. 416 E. coli have also been observed to shift to the seemingly less efficient yet faster metabolic 417 pathways under high substrate concentrations [e.g., Flamholz et al., 2013; Labhsetwar et al., 418 2014]. Depending on the details to be represented, we acknowledge that there are multiple ways 419 to model such phenomenon even with the circuit analogy. We next present one of these 420 mathematical explanations to show that, under certain aerobic conditions, high glucose 421 concentration makes fermentation more favorable.

422 According to the schema in Figure 6b, the specific ATP generation rate from the 423 fermentation pathway is

$$v_{FM,ATP} = \frac{Y_{FM}}{\frac{1}{f_S} + r_{fm}},\tag{38}$$

424 where  $f_s$  is the incoming flux of pyruvate (produced from glycolysis) sensed by the two 425 metabolic pathways (which is proportional to the incoming glucose flux sensed by the organism 426 under steady-state),  $r_{fm}$  is the resistance associated with the conversion of pyruvate into 427 fermentation products (which could be lactate, ethanol, or acetate depending on the organism; 428 [*Madigan et al.*, 2009]), and  $Y_{FM}$  is the ATP yield of fermentation. Similarly, the specific ATP 429 generation rate from the aerobic respiration pathway is

$$v_{AO,ATP} = \frac{Y_{AO}}{\frac{1}{f_S} + r_{cac} + r_{etc} + \frac{1}{f_{O2}}},$$
(39)

430 where  $r_{acc}$  and  $r_{etc}$  are resistance associated with the citric acid cycle, and the electron transport 431 chain, respectively.  $f_{02}$  is the incoming oxygen flux, and  $Y_{A0}$  is the ATP yield of aerobic 432 respiration. Because the citric acid cycle involves many more enzyme-catalyzed steps than 433 fermentation,  $r_{cac} > r_{fm}$ . Meanwhile,  $Y_{A0}$  is about 20 times the value of  $Y_{fm}$ [*Madigan et al.*, 434 2009].

In a metabolically active organism, for fermentation to be more favorable than aerobicrespiration, the following condition needs to be satisfied,

$$\frac{Y_{FM}}{Y_{AO}} > \frac{\frac{1}{f_S} + r_{fm}}{\frac{1}{f_S} + r_{cac} + r_{etc} + \frac{1}{f_{O2}}} > \frac{r_{fm}}{r_{cac} + r_{etc} + \frac{1}{f_{O2}}},\tag{40}$$

where the term after the second ">" suggests that fermentation is more favorable only when 437 oxygen is below a certain level of availability (note that  $f_{02}$  is approximately proportional to 438 439 diffusion). When the oxygen availability is sufficiently low, higher substrate concentration (i.e., greater  $f_S$ ) will make fermentation more effective in generating ATP. If we further consider that 440 441 the fermentation pathway requires the organism to maintain a much smaller number of enzymes 442 than required for the aerobic oxidation pathway (which is equivalent to increase the value of  $Y_{FM}/Y_{AO}$ , making the inequality (40) easier to be satisfied), we can expect fermentation to be 443 444 preferred for high supply of glucose (i.e., greater  $f_S$ ) even under certain aerobic conditions. (For 445 anaerobic condition,  $f_{02}$  approaches zero, and the inequality (40) is easily satisfied). Given the 446 significance of this problem in various contexts, including methane and hydrogen dynamics in 447 environment and industrial biogeochemistry [Lu et al., 2009; Madigan et al., 2009], we expect to 448 study this problem in a more quantitative and extensive way elsewhere.

Another very interesting application is to qualitatively explain why Monod kinetics canfit the substrate-growth rate relationship of an exponentially growing bacterial population

451 [Monod, 1949]. The argument goes like the following. For an exponentially growing bacterial 452 population, the bacteria proteomes are in steady state. Meanwhile, from the Ohm's law analogy 453 described here, we know that any functioning circuit-network can be equivalently represented by 454 a bulk resistor. Therefore, we contend that however complex the circuit representation of a 455 bacterial metabolism would be, it as a whole can be equivalently represented by a resistor  $r_E$ . 456 When this  $r_E$  is combined with the resistance associated with the incoming substrate flux (see 457 equation (7)), we say that the bacterial growth would very likely follow the Monod kinetics. 458 However, when the bacteria are in transition from one metabolic state into another, extra 459 resistors are introduced accompanying the change of proteomes, and Monod kinetics will fail for 460 such situations [e.g., Erickson et al., 2017]. This argument also explains why models based on 461 flux balance analysis with proteomic constraints can simulate steadily growing E. coli and yeast 462 realistically [Labhsetwar et al., 2014; Labhsetwar et al., 2017].

#### 463 **3.6 Limitations of the Ohm's law analogy**

464 While the Ohm's law analogy can be used to model many challenging biogeochemical 465 processes, it is not appropriate for all types of networks. For instance, it is not able to properly 466 couple two or more consumers (i.e., two or more batteries) within a single circuit network, even 467 though the electric-circuit theory itself does not forbid such a configuration to occur (which can 468 be solved with the Kirchhoff's law of voltage and current [e.g., Feynman et al., 2011a]). Rather, 469 such coupling can only be done by first representing the substrate dynamics of each consumer 470 separately, and then coupling them together by differential equations. Such coupling could be 471 critical when many consumers are competing for a limited substrate, even though none of the 472 consumers is substrate-limited when other consumers are excluded [e.g., Etienne et al., 2020]. 473 The equilibrium chemistry approximation (ECA) kinetics [Tang and Riley, 2013] and its progeny

SUPECA kinetics [*Tang and Riley*, 2017] are more capable of resolving such situations. In soil biogeochemistry, one such situation is to model the interaction of a substrate molecule (e.g., ammonium, inorganic phosphorus, or dissolved organic carbon) that is simultaneously undergoing uptake by organisms and adsorption by mineral surfaces. Fortunately, a simple remedy is possible for the Ohm's law analogy from the ECA kinetics. In the ECA kinetics, microbial uptake of substrate *S* under the influence of adsorption by mineral surface *M* (with affinity parameter  $K_M$ ) is

$$F = \frac{v_{max}SB}{K+S+MK/K_M + \alpha B'},\tag{41}$$

481 where *K* is the half saturation constant for the uptake of *S* by microbe *B* in the absence of *M*, and 482  $\alpha B$  is the within-population competition effect introduced by ECA. *Tang and Riley* [2019a] 483 showed that  $\alpha B$  is negligible due to the large size contrast between microbes (and likewise fine 484 roots) and substrate molecules. When  $\alpha B$  is ignored, equation (41) becomes

$$F = \frac{B}{\frac{1}{v_{max}} + \frac{1}{k_f S} \left( 1 + \frac{M}{K_M} \right)} = \frac{B}{\frac{1}{v_{max}} + \frac{1}{k_f^* S}},$$
(42)

485 with

$$k_f^* = k_f / \left(1 + \frac{M}{K_M}\right). \tag{43}$$

Now the Ohm's law analogy will still work if  $1/k_f^*S$  is used to defined the substrate dependent resistance. Moreover, equation (43) suggests that mineral surfaces may slow the microbial uptake of substrate *S* by effectively reducing the substrate delivery rate towards the microbes. However, when the sizes of substrates and competitors are similar (e.g., in some predator-prey relationships), the Ohm's law analogy will be too cumbersome to apply, and the ECA or SUPECA kinetics should be used. Nonetheless, it will be very interesting and helpful to 492 construct and compare models for the same system using both the Ohm's law analogy and ECA493 (or SUPECA) kinetics.

### 494 4 Conclusions

495 By applying the mathematical similarity between the Ohm's law and Michaelis-Menten 496 kinetics, we show that the electric circuit analogy can be used to derive many interesting results 497 of biogeochemical kinetics. We show this approach reproduces many successful applications in 498 the literature, including aerobic heterotrophic respiration, multi-nutrient co-limited microbial 499 (and plant) growth, denitrification dynamics, etc. This approach also sheds new insights on the 500 Warburg and Crabtree effect in prokaryotes and eukaryotes, and conceptually explains why the 501 Monod relationship accurately represents the kinetics of steadily-growing bacterial populations, 502 and why flux balance modeling with proteomic constraints is able to accurately model microbial 503 growth. Based on these results, we expect that the Ohm's law analogy will help build a unified 504 kinetic modelling framework of microbial and plant biogeochemistry to make more robust 505 predictions.

#### 506 Data Availability Statement

507 Data is available through *Shaver and Melillo* [1984], *Droop* [1974], *Franzluebbers* [1999], and
508 *Doran et al.* [1990].

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521	JYT conceived the idea and did the analysis; JYT, WJR, GLM and ELB discussed the analysis
522	and wrote the paper.
523	
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